

## 1. **PREAMBLE**

Ship's name	LPG/C VENTURE GAS
Owners	VENTURE GAS SHIPPING S.A
Flag - Registry	LIBERIA
Builder	1990 / KAWASAKI HEAVY INDUSTRIES
Delivery	28/06/1990
Class	NKK
IMO No.	8818207

GT (International)	42465
NT (International)	15521
GRT (Suez)	44359.27
NRT (Suez)	37291.81
GRT (Panama)	N/A
LWT (MT)	16430

Is vessel approved?		
USCG	NO	
IMO	YES	

# 2. HULL

	Metres	Feet
LOA	224.05	735.07
LBP	212.47	697.08
Breadth	36	118.1
Depth	20.70	67.91
Air draft (fm Summer LL)	37.34	122.48

	Draft (m)	Corresponding DWT
Tropical	11.248	51235T
Summer	11.019	49701T
Winter	10.79	48171T

TPC fully loaded (MT)	66.90T	



Estimated Mean draft with full bunkers and 98% cargo & full bunkers			
Cargo	Mean draft (m)	DWT	displacement
BUTANE	10.7M	47759.8	68880
PROPANE	10.48	46285.8	70040

## 3. COMMUNICATION EQUIPMENT

International call sign	D5QJ3
Radio station	JRC NDZ-227
Inmarsat F33	N/A
- Telephone FBB	+870 773309821
- Telephone	N/A
- Telefax	+870 783320640
- Telex	636018584 VENTURE X
Inmarsat C	463724934@stratosmobile.net
MMSI	636018584
Cell phone	N/A
E-Mail	master.venturegas@amosconnect.com

## 4. **MACHINERY**

Main Engine		
Maker/model	KAWASAKI MAN - B&W 5S70MCE	
MCR	12400BHP AT 80 RPM 9120KW	
Grade fuel used	380 CST AT 50°C	

Auxiliaries Engines		
Type/Model	T 260L-ET	
Maker	YANMAR DIESEL	
Output(KW/RPM)	1000KW	
Generator	3 UNIT	
Grade fuel used	380 CST AT 50°C	



Speed		
Guarantee average loaded/ ballast speed (kt) 13KN		
Draft at Guarantee average loaded/ ballast speed (m)	11.60m / 7.50m	

Consumption			
	Consumption at sea	Consumption at port	
Main engine (IFO)	13 knts : 27.5T / 25.8T(Ballast)	ÑA	
Aux. Engines (IFO)	6.0T	3.0 T	
Number of A/E in use	2	1	

MDO Consumption alongside in port	NA	NA
Inert Gas plant when operating	5T	
Boiler consumption (MT/day)	2T	

Permanent bunkers capacity (Excl. daily service tanks) @ 98%		
HFO (MT ) 2166.87		
MDO (MT )	649.93	

## 5. **CARGO INSTALLATION**

Re-liquefaction plant Type	2 STAGE DIRECT TYPE OIL FREE
Minimum temperature can maintain	-45C

Tank No.	Capacities		BUTANE 0.580 @	PROPAN E 0.5085	<b>Ethylene</b> 0.5653	NH3 0.682 @	Butadien e 0.653
	100% M <sup>3</sup>	98% M <sup>3</sup>	-3° C	@ -41.0° C	-101.5	-33.4° C	@ -5°C
1	14980.878	14798.470	8850	8557	NA	NA	NA
2	20112.232	19856.224	11876	11481	NA	NA	NA
3	20135.912	19875.268	11895	11500	NA	NA	NA
4	19979.146	19718.458	11793	11402	NA	NA	NA
Total	75208.168	74248.420	44414	42940	NA	NA	NA

Carried Products
BUTANE (UN1011)
PROPANE (UN1978)
LPG MIX (UN1011 / 1978)



## Cooling before loading

(for fully-refrigerated vessels what quantity of cargo is needed and which is the corresponding time to pre-cool the tanks and have them ready to load?)

corresponding time to pro-coor the tarme and have them ready to read )				
NA	MT	Hrs		
PROPANE	400	24 HRS.		
BUTANE	400	20 HRS.		

### 6. **CARGO TANKS**

Туре	INDEPENDENT TANK TYPE A		
Material		CARBON MANGANESE STEEL	
MARVS		0.25 Kg/cm2	
WARVS		-0.07 Kg/cm2	
Maximum Vacuum	1	-0.07 Kg/cm2	
Minimum pressure		0.02 Kg/cm2	
Minimum tempera	ture acceptable in tanks -45C		
Maximum Specific	ic Gravity 0.6050		
Maximum Loading	rate – m³/hour	With vapour return:	
		BUTANE:4000M3/HR -	
		PROPANE:4000M3/HR	
		Without vapour return:	
		BUTANE: 3000M3/HR	
		PROPANE: 1500M3/HR	
Number of deck ta	nks	N/A	

## 7. CARGO PUMPS

Number/Type	8 X 600 M3 / VERTICAL ELECTRIC MOTOR DRIVEN SUBMERGE CENTRIFUGAL FIXED TYPE			
Maker		SHINKO IN	IDUSTRIES	
Location		AT AFT BOTTOM OF CARGO TANK		
Max permissible	ible specific gravity 0.5791 @15 C			
Cargo remaining onboard in cargo tanks after total completion pumping		280 MT		
Cargo remaining onboard in cargo tanks		35 MT		
(heel) after completion pumping				
Total head when booster pump	n working in series with	120mlc		



Booster pumps (number/type)	1 / CENTRIFUGAL
Maker	HAMWORTHY SVANEHOJ (500m <sup>3</sup> )

Stripping		
Stripping system	DRIVE BY MAIN CARGO	
	PUMPS	
Time required for all liquid cargo	126 HRS BY EDUCTOR	

Loading Rates			
Loading rate (with vapour return) -BUTANE	4000T/H		
Loading rate (with vapour return) – PROPANE*	4000T/H		
Loading rate (without vapour return line) – PROPANE	1500T/H		
Loading rate (without vapour return line) – BUTANE	3000T/H		

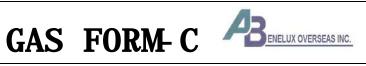
(\*)Note: for pressure or semi-refrigerated vessels using the cargo heater with sea temperature  $+15^{\circ}$  C

Time for discharging full cargo using all pumps against no backpressure				
With vapour return Without vapour				
line (hours) return line (hours				
Discharging rate (atm)	17.5 HRS.	17.5 HRS.		
Discharging rate (1 bar)	17.5 HRS.	17.5 HRS.		
Discharging rate (5 bars) 22.0 HRS. 22.0 HRS.				
Discharging rate (10 bars)	N/A	N/A		

### 8. **CARGO COMPRESSORS**

Number/Type	4 /2K 160-2F
Maker/Model	SULZER BURCKHARDT
Total Swept volume	PROPANE = 1026m3/hr. 171700kCAL
	BUTANE = 1395m3/hr. 251100 kCAL
Can re-liquefy VCM	N/A

	Ethylene	Propane	Butane
Refrigeration	NA	1026 m3/hr	1395 m3/hr
Capacity		171700Kcal	251100 kCAL
Suction pressure	NA	0.2	0.2



## 9. **INERT GAS SYSTEM**

Does the vessel use inert gas?	YES
Method	FLUE GAS
Maker	GADELIUS
Fuel used	MDO

Does the vessel produce inert gas?	YES
Туре	NA
Daily production	5000 M3/HR

Composition of inert gas		
Carbon dioxide	ABT. 15 %	
Oxygen max.	MAX 0.5 %	
Carbon monoxide max.	MAX 1000 PPM	
Hydrogen max.	MAX 1000 PPM	
Nitrogen	BALANCE	
Soot	0	
Suphur oxides max.	MAX 50 PPM	
Dewpoint	+5 °C - SATURATED AT SPECIFIED TEMP. /	
-	PRESS.	

State if any shore supply of liquid nitrogen may be required		
May be required for pumping tanks prior to loading butadiene and		
ammonia		
What quantity?	N/A	

## 10. GAS FREEING

Can this operation be carried out at	YES
sea?	TES

State method incl. all details		
For LPG	PUDDLE HEATING / INERTING / AERATING	
For NH <sub>3</sub>	N/A	

Advise time required and consumption of inert gas if any		
From LPG about 108 HRS./ 100,000 m3		
From NH <sub>3</sub>	N/A	
Is the vessel equipped with inert gas	YES	
blower?	TES	
Capacity	5000 M3/HR	



Ventilation fan	20000M3/H		
11. CHANGING GRADE			
Can this operation be carried out at	VEC		
sea?	YES		
State method used and time required for charging from NH <sub>3</sub> to LPG and			
vice versa, to reach 50 ppm to previou	s cargo in tanks atmosphere, the		
tanks being dry and free of moisture (dewpoint plus 10° C)			
From NH₃ to LPG	N/A		
Time required	N/A		
From NH₃ to LPG	N/A		
Time required	N/A		
Can vessel reduce in tank			
atmosphere and gas installation	N/A		
concentration of previous cargo	IV/A		
below 50 ppm?			
Method used, time required and	N/A		
extra shore supply if any	<u> </u>		
How can it be checked that no liquid	Remote temperature sensor at tank		
gas remain onboard	bottom		

## 12. CARGO HEATER

Cargo Heater	1	
Maker	HAMWORTHY (	GAS SYSTEM
Туре	SEAWATER TYPE TUBE DIRECT	
Discharging rate for C3 & NH3 to be brought	500M3/H	N/A
fm atmospheric pressure to -5° C @ S.W 15° C		
State discharging rate for propane with 2.5 mol brought from -44oC to -5oC at sea temperature	500M3/H	

## 13. CARGO VAPOURIZER

In case of need of vapour gas during discharge, can	YES CARGO
vessel produce its own if no shore gas available?	VAPOURISER
	EXISTING

## 14. **REFRIGERATING APPARATUS**



It is independent of cargo?	YES
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### 15. **MEASURING APPARATUS**

What gauges onboard	ELECTROMAGNETIC FLOAT TYPE
Location and type	CARGO CONTROL ROOM
Number of temperature sensors/gauges per tank	7/2
Number of pressure sensors/gauges on tank	3/3

## 16. **SAMPLES**

Where samples can be taken?	FROM TANK DOME SAMPLE POINT
Are sample bottles available	NO
onboard?	NO

## **CARGO LINES** 17.

Is vessel fitted with midship manifolds	YES
Number of lines on each side	4
Lines Configuration	V/L/L/V
Distance from cargo manifold to bow	115.95 M
Distance from manifold to stern	108.1 M
Height upper cargo manifold above main deck	1.7M
Height above Summer Draft mark	11.731 M
Height upper cargo manifold waterline when LWT	15.781 M
Height upper cargo manifold above waterline when in ballast	15.45 M
Distance manifold from ship's rail	2970 MM
Distance between liquid lines	2400 MM
Distance between vapour lines	7200 MM
Distance between loading and vapour return connections	2400 MM
Is vessel fitted with stern discharge	N/A
Is vessel fitted with fore discharge	N/A

Note: Above distances from center line of liquid and vapour crossovers



Dimension of lines			
	Diameter Flange size		
Liquid (P/S)	400mm	300mm	
Vapour	300mm	200mm	
Booster	N/A	N/A	

	What reducers onboard		
Number of reducer	Diameter	Length	Pressure rating
1	16 X 150 / 12 X 150		
1	16 X 300 / 12 X 300		
1	16 X 150 / 10 X 300		
2	14 X 150 / 12 X 150		
1	12 X 300 / 12 X 300		
1	12 X 300 / 12 X 150		
3	12 X 150 / 12 X 150		
1	12 X 300 / 10 X 300		
1	12 X 300 / 10 X 150		
2	12 X 150 / 10 X 150		
1	12 X 300 / 8 X 300		
6	12 X 150 / 8 X 150		
1	12 X 300 / 6 X 300		
1	12 X 300 / 6 X 150		
2	12 X 150 / 6 X 150		
2	10 X 150 / 8 X 150		
1	8 X 150 / 8 X 150		

# 18. LIFTING APPLIANCES

Where situated	MID SHIP CRANE
Number and lifting capacity	1 X 5T SWL
Max. distance from ship's side of lifting hook	4.5M

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## 19. **HOSES**

For what products are hoses suitable				
Number	Length	Diameter	Working pressure	Flange
NA				
NA				

## 20. **SPECIAL FACILITIES**

How many grades can vessel segregate? 2 GRADES (Tk2 & Tk4 must be of SAME GRADE)		
Indicate systems SYSTEM 1 / SYSTEM 2		
Is vessel able to load/discharge two	YES / 2 GRADES	
or more grades simultaneously?	TEO / Z ONADEO	
Can vessel sail with slack tanks?	YES	
Is vessel fitted with purge tank?	NO	